# ORIGINAL ARTICLE

# A comparative review of hydrologic issues involved in geologic storage of CO<sub>2</sub> and injection disposal of liquid waste

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**Abstract** The paper presents a comparison of hydrologic issues and technical approaches used in deep-well injection and disposal of liquid wastes, and those issues and approaches associated with injection and storage of CO<sub>2</sub> in deep brine formations. These comparisons have been discussed in nine areas: injection well integrity; abandoned well problems; buoyancy effects; multiphase flow effects; heterogeneity and flow channeling; multilayer isolation effects; caprock effectiveness and hydromechanics; site characterization and monitoring; effects of CO<sub>2</sub> storage on groundwater resources. There are considerable similarities, as well as significant differences. Scientifically and technically, these two fields can learn much from each other. The discussions presented in this paper should help to focus on the key scientific issues facing deep injection of fluids. A substantial but by no means exhaustive reference list has been provided for further studies into the subject.

#### Introduction

gases (DOE 1999a) through injection of anthropogenic CO<sub>2</sub> into deep brine formations is being actively studied, both in the USA and internationally. If this technology is to be deployed broadly enough to make a significant

Reduction of net atmospheric emissions of greenhouse

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impact on global emissions of CO<sub>2</sub>, thousands of wells, each injecting large quantities of CO2, will be needed. For example, in the US alone, the coal-fired electric generating capacity in 1999 was 278,000 MWe (DOE 1999b). Since CO<sub>2</sub> emission is reported to be about 800 kg per KWh (Rao 2007; Energy Information Administration 2005; see also Blasing et al. 2005), a single coal-fired power plant with 1,000-MWe capacity generates about  $19 \times 10^6$  kg or 19,000 tonnes of CO<sub>2</sub> per day. This corresponds to about seven million tonnes of CO<sub>2</sub> per year for the one 1,000-MWe plant. The large scale of effective CO<sub>2</sub> geological storage suggests the need for a careful evaluation of technical issues associated with this endeavor. Such an evaluation should specifically include the identification and incorporation of the best CO<sub>2</sub>-injection practices, the best scientific understanding of migration in subsurface formations, and the development of monitoring technology to ensure that geologic sequestration is safe and effective.

In this effort, it is useful to review the extensive history (over the last 50 years or so) of liquid waste injection into geologic formations in the US (Apps and Tsang 1996; Tsang and Apps 2005). Many of the hydrologic issues involved in injection disposal of liquid waste and injection storage of CO<sub>2</sub> are similar, although there are some significant differences. The purpose of the present paper is to review these common hydrologic issues, and to evaluate whether studies of CO<sub>2</sub> geologic storage can draw on some experiences from liquid-waste injection. The emphasis is on the issues and methodologies, rather than quantitative comparisons of characteristics between the two cases. In the following sections, we first give a brief history of liquid-waste injection in the US. Then, the special physical and chemical characteristics of CO<sub>2</sub> (in contrast to liquid waste) are discussed, and the relevant hydrologic issues



and technical approaches involved in the two cases are compared.

# Brief history of liquid-waste disposal by deep injection wells in the United States

The practice of using injection wells for waste disposal started in oil fields during the 1930s, when depleted reservoirs were used for the disposal of brines and other waste fluids from oil and gas production (Clark et al. 2005; Brasier and Kobelski 1996). The first report on injection of industrial waste was published in 1939 (Harlow 1939). The literature indicates only four such wells in 1950. A 1963 inventory by the US Bureau of Mines listed 30 wells (Donaldson 1964). Most of these early wells were converted oil production wells. By the early 1970s, the number of injection wells had grown to approximately 250 (Warner 1972), and they were being used to dispose of municipal sewage effluent as well as industrial wastes. A number of well-integrity failures in the 1960s and 1970s have been documented (Lehr 1986). These included contamination of a drinking water aguifer in Beaumont, TX, USA, caused by an injection well that did not have a separate injection tube within the well. The injected waste caused corrosion of both the inner and outer casings and the surrounding layers of cement, resulting in leakage from the injection well. In Odessa, TX, USA, an injection well was clogged owing to precipitation from interaction between two incompatible waste streams, and surface injection pressures quickly exceeded the allowable limits. In Denver, CO, USA, injection activated seismic events in a fault zone, which allowed injected liquids to escape through rock fractures and facilitated earthquake activities (Hsieh and Bredehoeft 1981; Wesson and Nicholson 1987).

Concerns about the safety of deep injection disposal in the US Congress motivated the US Environmental Protection Agency to develop regulations in the 1980s and 1990s, and to set requirements and standards for underground injection of liquid waste (Brasier and Kobelski 1996). These requirements included a well-designed and carefully monitored construction of injection wells and periodic testing of their integrity. They also included a demonstration, through the use of computer models, that the contained hazardous wastes would not migrate out of the injection zone for at least 10,000 years. This demonstration could be based on models of flow and waste transformation within the injection zone. Since the setting of these standards, no significant well failures have occurred. By 2000, there were 485 deep injection wells in the US for disposal of industrial liquid waste (Clark et al. 2005), and the depth of injection zone ranges typically from 1,500 to 2,500 m (see e.g., Mercer et al. 2005).



# Hydrologic issues related to CO<sub>2</sub> injection storage and liquid-waste injection disposal

CO<sub>2</sub> sequestered by injection in a deep brine formation (e.g., about 1,000 m) would be stored in three forms: a dense supercritical gas phase, a dissolved state in pore water, and an immobilized state through geochemical reaction with in situ minerals (Hendriks and Blok 1993: Bachu et al. 1994). The fraction of pore space estimated to be available for sequestration varies widely, from the 2 to 6% estimated by van der Meer (1995) to the range of 20-30% calculated by Pruess et al. (2001a). The dissolvedstate CO<sub>2</sub> at equilibrium is estimated to range from 2% in saturated NaCl brines to 7% in dilute water. CO2 immobilization in formation matrix minerals is a very slow process and varies considerably with rock types. The amount of CO<sub>2</sub> sequestered through such mineral reactions can be comparable to CO<sub>2</sub> dissolution in pure waters. Thus, among all three forms of CO<sub>2</sub> sequestration in the injection brine formation, the supercritical gas phase is the main storage form, with properties quite different from those of pore water in the injection formation. Thus, for storage of CO<sub>2</sub> at 1,000 m depth, its density is about 60-75% that of water in the formation, and its viscosity is about 15-20 times less than that of water (Vargaftik 1975).

Figure 1 illustrates a basic scenario of injection and storage of  $CO_2$  in a brine formation, with a storage injection zone greater than 800 m in depth, overlain by a caprock. Three main physico-chemical processes are indicated. First, there is the hydrologic process of density-driven or buoyancy flow for the supercritical  $CO_2$  with a lower density and an order-of-magnitude (or more) lower viscosity. Thus, the plume of injected  $CO_2$  migrates outward from the injection well and up toward the caprock via buoyancy, with a large spread in terms of surface area.

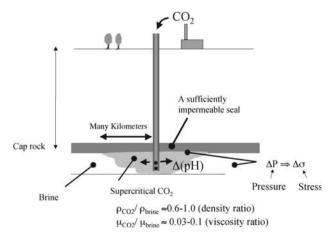


Fig. 1 A general sketch of hydrophysical processes associated with  $CO_2$  injection in a deep brine formation

Such density-driven flow also operates in the formation fluid with dissolved  $CO_2$  since its density will also be different from the initial formation brine. In this case, the density of  $CO_2$ -saturated brine will be higher and it will flow downward. In contrast, for liquid-waste injection, the density tends to be within 10% of that of the formation brine, and the viscosity is about the same—thus, the buoyancy effect is significantly less. At the caprock, both waste liquid and injected  $CO_2$  are hindered from flowing upward. However, for  $CO_2$ , there is an additional effect of gas entry pressure that acts as a threshold to prevent the  $CO_2$  to enter into the pores of the water-saturated caprock.

Second, for liquid injection, with respect to the mechanical responses of the system, only the injection pressure needs to be considered for hydromechanical effects such as hydrofracturing. The mechanical impact is mainly in the immediate vicinity of the injection well, because injection pressure decreases rapidly with radial distance. For the CO<sub>2</sub> case, however, both injection and buoyancy provide additional stress on the rock. For injection pressure, the impact is similar to that of the liquid injection case. But buoyancy pressure operates where the CO<sub>2</sub> is, which can be over a very large area, both because of the large volume of CO2 that needs to be stored and because of its spread as a result of buoyancy flow. In response to these pressures, the rock matrix may be deformed, with changes in the values of matrix porosity, and, if fractures are present in the injection formation or the caprock, possible changes in fracture apertures may occur as well. These changes, in turn, may cause variations in flow permeability and, consequently, the flow field. Finally, in general, the injected CO<sub>2</sub> plume interacts chemically with the formation minerals. For example, exsolution of CO<sub>2</sub> from water along a pressure-temperature gradient might cause precipitation of carbonate minerals. Such interactions could give rise to local porosity and permeability changes and modify medium heterogeneity (see, e.g., Ross et al. 1981; Mathis and Sears 1984), but positively, such chemical changes can also react with the injected CO<sub>2</sub> to form new minerals in the rock matrix, thus trapping the CO<sub>2</sub> chemically.

# Injection well integrity

As can be seen in "History of liquid-waste injection wells" section above, problems associated with well integrity were historically the main mode of failure in deep-well injection of liquid waste (Lehr 1986). Thus, construction of properly designed injection wells is one of the main concerns (Bundy and Fizer 1996). Figure 2 shows a typical injection-well design required for deep injection of hazardous liquid waste (Brasier and Kobelski 1996; Rish 2005). The well, as shown in this figure must

have at least two strings of casing. The so-called surface casing is cemented to the land surface and is designed to isolate the well from the shallower aquifers of drinking water. The second casing, labeled "protection casing" in Fig. 2, extends all the way to the injection zone and is cemented to ensure no cross flow between adjacent brine formations. Furthermore, an injection tubing is set into a packer, which is a mechanical device set in the well to isolate the injection zone, to ensure that injection via the tubing is emplaced in the target injection zone. Materials, in particular the cement used in the construction of the injection well, must be resistant to corrosion caused by injected liquids or formation brines (Whiteside et al. 1996; Kelly and Fleniken 1996).

The design of injection wells for CO<sub>2</sub> storage will have to be carried out with similar considerations (Gerard et al. 2006). In fact, because of the corrosive properties of CO<sub>2</sub> and the expected long life of CO<sub>2</sub> injection wells—with an operation period of 25–100 years and a safety period of 1,000 years or more—evaluation of materials for well integrity will be even more stringent (IEA 2005). Fortunately, we have extensive experience in enhanced oil recovery (EOR), which has been reviewed in a general discussion on CO<sub>2</sub> injection well integrity under the auspices of International Energy Agency (IEA 2005), and also in acid gas injection (for example in Canada) over the last 10 years or so (Bachu et al. 2005). From these areas, the transfer of technology and knowledge to CO<sub>2</sub> injection and storage is possible.

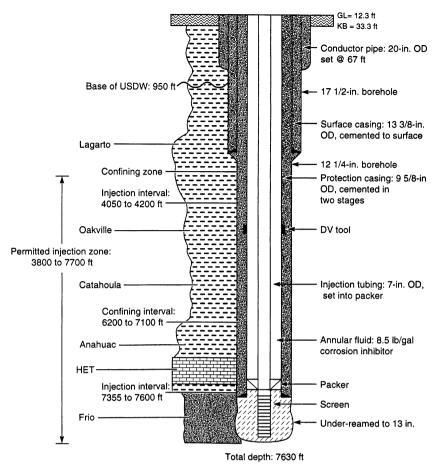
#### Abandoned wells

Abandoned wells are a concern for deep-injection disposal of liquid wastes. Part of site selection for liquid-waste injection is to ensure that there are no abandoned wells within the so-called area of review around the injection well (see, e.g., Platt and Rectenwald 2005; Rish 2005). If there are, then special effort must be taken to investigate and improve their condition, if necessary, so that they will not act as leakage paths for the injected liquid. One problem is that records of old abandoned wells are sometimes nonexistent or lost, and research has been conducted to develop the capability to detect these wells by geophysical or other means. It turns out that the amount of liquid waste injected deep underground is limited, so that the area of review is not too large, on the order of 100s to 1,000s of meters in radius. Furthermore since the driving force for leakage of liquid waste is the injection pressure, which is largest close to the injection well and decays quickly as a function of radial distance, the region of most concern is liable to be close to the injection well.

For CO<sub>2</sub> injection and storage, on the other hand, the region of concern will be larger. First, the area covered by



Fig. 2 A typical injection well design required for deep injection of hazardous liquid waste [prepared by DuPont Company and shown in Brasier and Kobelski (1996) and Rish (2005)]



the injected CO<sub>2</sub> will be very large, with a radius perhaps of tens of kilometers—not only because a large volume of CO<sub>2</sub> must be stored, but also because the buoyancy effect causes the CO2 plume to move upwards and spread out farther. Second, the driving force for CO2 leakage is not just the injection pressure, but also the buoyancy force, so that the leakage potential exists wherever CO<sub>2</sub> migrates. Celia et al., in a series of papers (Celia et al. 2005, 2006a, b), studied the problem in some detail. They pointed out that one type of region for CO<sub>2</sub> storage is mature sedimentary basins, some of which have undergone oil and gas exploration over the last century. In these basins, there are a large number of wells. For example, in Texas, USA, more than 1 million wells have been drilled; and in Alberta, Canada, more than 350,000. Celia et al. (2006b) estimated that, in high well-density areas, a CO<sub>2</sub> plume with a radius of about 5 km would come into contact with several hundred wells, and with tens of wells even in low well-density areas. The former (high well-density areas) correspond to areas where productive oil and gas wells have been found and the latter (low well-density areas) where hydrocarbon resources have not been found.

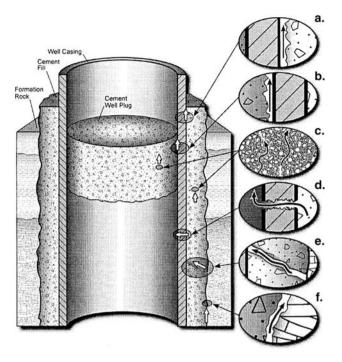
When CO<sub>2</sub> encounters a well without proper plugging, it will tend to migrate upwards under buoyancy force. When a well is abandoned prior to development for oil or gas

production, it would typically be filled by a series of cement plugs. If it were abandoned after development and oil or gas production, it would have a casing, with cement emplaced not only in the hole within the casing, but also in the annular space between the case and the borehole. Figure 3 shows the possible leakage paths in such an abandoned well, which include preferential flow pathways along rock-cement and casing-cement interfaces, as well as through degraded materials or materials improperly formed during the plugging processes (Celia et al. 2005). Longlasting cement that can withstand the corrosive effects of CO<sub>2</sub> is currently an active area of research in CO<sub>2</sub> storage (see, e.g., Strazisar and Kutchko 2006). It is needed not only for plugging abandoned wells but also for plugging injection wells at the end of their service. This kind of problem has also been considered for liquid-waste injection (Whiteside et al. 1996). One advantage for liquid waste is that because of the relatively much smaller volume involved, it is possible to pre-treat the liquid waste to moderate its corrosive characteristics.

## Buoyancy effect

As pointed out above, buoyancy effects are much more important for CO<sub>2</sub> than for the liquid-waste injection case.





**Fig. 3** Possible leakage paths in an abandoned well (Celia et al. 2005). Leakage paths include those at well plug-well casing interface (a), well casing-cement fill interface (b), and cement fill-formation rock interface (f), as well as flow lines through cement itself (c), and through cracks in the well casing and cement fill (d, e)

Nevertheless, questions on their impact on potential migration of injected waste have been raised concerning injection of liquid that is denser or lighter than the in situ brine. These questions that have stimulated many studies (see, e.g., Samsonova and Drozhko 1996; Tsang 1996). Hellström et al. (1988) presented a formula for a dimensionless measure  $\gamma$  of forced convection flow compared with buoyancy flow as

$$\gamma = \frac{Q\langle \mu \rangle}{Bg\Delta\rho\sqrt{k_x}k_z}$$

where Q is the injection flow rate,  $\langle \mu \rangle$  is the mean viscosity between the injected liquid and the formation brine, B is the injection zone thickness, g is the gravitation constant,  $\Delta \rho$  is the density difference between the injected fluid and the formation brine, and  $k_x$  and  $k_z$  are the permeabilities in the x and z directions, respectively.

This formula is essentially the same as the ratio of viscous to gravity effects  $R_{\rm v/g}$  divided by the parameter accounting for anisotropy  $R_{\rm L}$ , given by Ennis-King and Paterson (2000) in their discussion of  ${\rm CO_2}$  injection and storage. It also corresponds to the dimensionless parameter group  $\Gamma$  proposed by Celia et al. (2005) for  ${\rm CO_2}$  injection, except that the  $\langle \mu \rangle$  factor is replaced by brine mobility, defined as the ratio of relative permeability to viscosity. In

addition, Celia et al. (2005) did not consider formation anisotropy, so that  $k_x$  and  $k_z$  were equal.

Because of the buoyancy flow of  $CO_2$  to the top of the injection zone, the areal extent of the injected  $CO_2$  will be larger than a buoyancy-neutral fluid. For example, storage of  $2.7 \times 10^{11}$  kg  $CO_2$  at the rate of 350 kg/s for 30 years in a 100-m thick formation, with isotropic permeability  $k = 10^{-13}$  m<sup>2</sup>, will have an increase in areal extent (due to buoyancy flow) of about 1.4 (Pruess et al. 2001b). In this example, because of the large volume of  $CO_2$  injected, the areal extent of the injected supercritical  $CO_2$  in the injection zone is as much as  $120 \text{ km}^2$ . A typical injection of liquid waste (Mercer et al. 2005) will have an areal extent that is one or two orders of magnitude smaller.

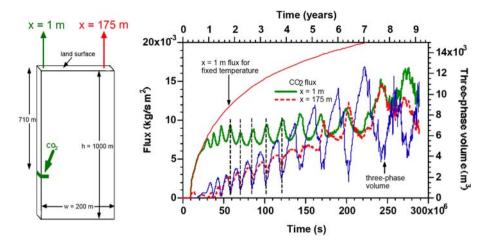
# Multiphase flow effects

Injection of liquid waste generally involves single-phase fluid flow, because the injected liquids are typically miscible with water. Injection of supercritical CO2 involves multiple phases. Along any potential leakage paths, three phases are present in varying proportions—namely, liquid water (with or without dissolved CO<sub>2</sub>), liquid or supercritical CO<sub>2</sub>, and gaseous CO<sub>2</sub>. These phases will interfere with each other, which is often described by three-phase relative permeability functions. These relative permeability functions may be different for a fluid that is receding (draining) or advancing (imbibing), and may further depend on the initial saturation level of the fluid. Much research is being done to better understand the three-phase flow behavior of CO2-brine systems (e.g., Bachu and Bennion, this issue; Chalbaud et al. 2006; Gallo et al. 2006; Pruess et al. 2004; Pruess and Garcia 2002; Chang et al. 1994).

Hydrothermal effects combined with those of phase transition between supercritical and gaseous CO<sub>2</sub> can lead to very complex flow processes. Figure 4 shows an example of the complex phase-interference effects during fast CO<sub>2</sub> discharge through a fault. The figure shows the results of a numerical simulation conducted by Pruess (2006) on a schematic model of a fault zone initially containing water at a geothermal equilibrium of 30°C/km in hydrostatic equilibrium, with the land surface maintained at 15°C (Fig. 4a). CO<sub>2</sub> is discharged at 710 m depth in the fracture with an overpressure of 10 bars. As the CO<sub>2</sub> flows up (through buoyancy) and expands, it experiences strong cooling resulting from the Joule-Thomson effect, which in turn results in CO2 existing in two phases, as gas and as liquid. The two CO<sub>2</sub> phases interfere with each other and with the liquid water, creating phase interference and a slowdown of the leakage. At slower leakage rates, the three-phase fluid is heated more effectively by the neighboring rock wall (which was at normal geothermal



Fig. 4 Simulation results on complex phase interference effects during fast CO2 discharge through a fault. The model design is shown on left and upward fluid fluxes as a function of time at two locations, x = 1 m and x = 175 m are shown on the right, together with occurrence of three-phase volume. The figure shows that a large threephase volume would reduce upward flux at x = 1 m, by pushing fluid to the side so that upward flux at x = 175 m is increased (Pruess 2006)



gradient), then part of the liquid CO<sub>2</sub> boils off, and the three-phase interference effect decreases. As a result, the simulations show a persistent flow cycling effect, with an increasing and decreasing leakage rate, after a period of initial growth, as shown in Fig. 4b. The importance of such a behavior on the performance or safety of CO<sub>2</sub> storage is yet to be determined, but the example demonstrates the significant difference in flow processes between liquid-waste disposal and CO<sub>2</sub> storage in the subsurface. It also indicates that the predictive modeling necessary for performance assessment of future sites is much more complex for CO<sub>2</sub> versus liquid-waste storage.

#### Heterogeneity and channeling flow

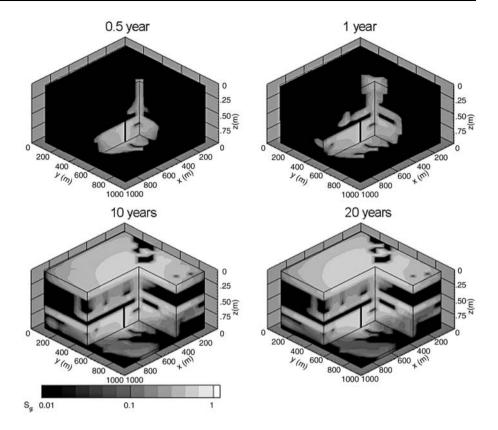
Heterogeneity is one of the factors that gives rise to fingering or channelized flow (Tsang et al. 2001; Pozdniakov et al. 2005), which increases the spread of liquid waste injected into a deep brine formation. Thus, the area of review for liquid-waste injection has to be larger than otherwise. Tsang (1996) presented a rough analytic estimate of such a spatial increase for liquid injection. Similar considerations on the spatial extent of stored CO<sub>2</sub> with the effect of heterogeneity are presented in Ambrose et al. (2006) and Doughty et al. (2001). However, for CO<sub>2</sub> injection storage, other factors come into play, so that heterogeneity may not be altogether negative. Flett et al. (2005, 2006) described heterogeneities of several types important for CO<sub>2</sub> storage; namely, stratigraphic layering within the storage formation, faults, depositonal mixing, compartmentalization, and channel systems. For example, stratigraphic layering counteracts buoyancy flow by limiting the flow to the injection zone and acting as a structural barrier. If CO<sub>2</sub> is injected into the lower part of the storage formation, heterogeneity (layering) may actually prevent it from migrating upward and coming near potential leakage paths in the caprock. This effect is evident in the seismic profiles taken at the  $CO_2$  injection site at Sleipner (Torp and Gale 2004). Furthermore, heterogeneity with flow channeling increases the contact between the brine formation and the injected  $CO_2$ , thus increasing the potential for  $CO_2$  solution and mineral trapping (Doughty et al. 2001).

To demonstrate the effects of heterogeneity on CO<sub>2</sub> storage, Doughty et al. (2001) conducted simulations on a geological model based on data from the Frio formation in Texas, USA, where a small-scale pilot test for CO<sub>2</sub> injection was conducted (Hovorka et al. 2004). A threedimensional (3D) stochastical model was constructed, with model layers derived from three idealized representations of fluvial depositional settings found in this part of the Frio-namely, barrier bars (continuous high-permeability sands), distributary channels (intermingled sands and shales, with a large high-permeability sand component), and interdistributary bayfill (predominantly low-permeability discontinuous shale lenses, interspersed with moderate-permeability sand). Figure 5 shows a model of  $1 \text{ km} \times 1 \text{ km} \times 100 \text{ m}$ , designed to represent part of the subsurface storage volume for a 1,000 MW power plant located near the site (called the Umbrella Point oil field). The top and bottom boundaries are closed to represent sealing shale layers. Lateral boundaries are held at a constant pressure. Carbon dioxide is injected at a rate of 21.6 kg/s (680,000 metric tons per year) for a period of 20 years; then the system is monitored for an additional 80 years to watch the evolution of the CO<sub>2</sub> plume. This injection rate represents about half of the CO<sub>2</sub> output from the 1,000-MW gas-fired power plant.

The figure shows that the interplay between geological heterogeneity and buoyancy flow is crucial in determining where and how effective structural and stratigraphic traps are. However, the heterogeneity-buoyancy interaction also strongly impacts the character of the subsurface CO<sub>2</sub> plume—that is, how CO<sub>2</sub> is distributed in space.



Fig. 5 Example of the role of heterogeneity on  $CO_2$  distribution in the storage brine formation after injection of 0.5, 1, 10, and 20 years (Doughty et al. 2001)



Low-permeability lenses provide flow barriers that may retard vertical buoyancy flow; but if the barriers are discontinuous, the buoyant CO<sub>2</sub> will move upward between them, creating a sinuous extensive plume. In contrast, for homogeneous sand, buoyancy flow simply drives the plume to the top of the formation, where it may collect in a compact shape or spread extensively along the lower boundary of the caprock.

Other hydrologic effects, such as dipping storage formations (Akervoll et al. 2006; Flett et al. 2006), have also been considered with respect to their impact on storage capacity and  $CO_2$  migration.

# Multilayer isolation effect

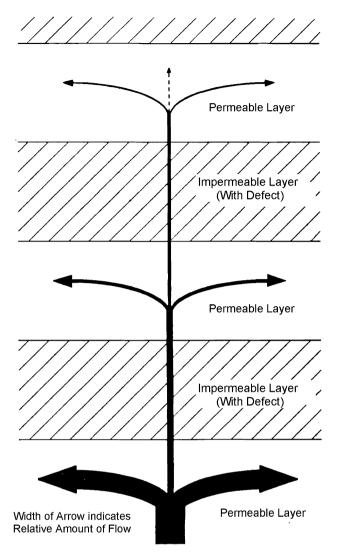
For liquid waste injection, the multilayer stratigraphy above a storage formation is usually not considered, because the site chosen is supposed to have an effective barrier that would prevent escape from the injection zone. Nevertheless, Miller et al. (1986), in their discussion of liquid-waste injection, did consider this case (Fig. 6) and suggested the benefit of having multiple low-permeability layers to ensure that the injected liquid would not reach the shallow subsurface.

For CO<sub>2</sub> injection, on the other hand, the benefit of isolating injected CO<sub>2</sub> through multiple layers of low-permeability layers has been recognized through the

Sleipner field studies (Torp and Gale 2004; Chadwick et al. 2004). Further, in contrast to liquid waste injection, some degree of CO<sub>2</sub> leakage may be unavoidable and can probably be acceptable, if it does not give rise to health, safety, and environmental concerns, and if the objective of reducing net greenhouse gas emission is achieved. With this in mind, a detailed analysis of the multilayered system needs to be made to evaluate the efficiency of injection-storage of CO<sub>2</sub>. For systems with leakage paths, the expected leakage rate is an important input to CO<sub>2</sub> storage performance and risk assessment. The results will also be needed to design a monitoring system for CO<sub>2</sub> storage (see section "Site characterization and monitoring" below).

As an example of such an effort, Fig. 7 presents the results of numerical simulations considering  $CO_2$  injection into a deep multilayer system with pre-existing faults. In the simulations,  $CO_2$  is injected at a rate of 0.04 kg/m/s over 30 years into a deep saline reservoir overlain by a sequence of two additional caprock units and two additional aquifer layers. One fault is assumed to intersect the lower caprock unit, about 1,000 m away from the injection well, while a second fault intersects the upper caprock unit at a 2,000 m distance from the first fault, on the other side of the injection well. The simulation study aimed at (1) determining the  $CO_2$  migration patterns in such a system, (2) evaluating the benefit of injecting into a multilayer system with possible attenuation of the migrating  $CO_2$ , and





**Fig. 6** A schematic picture of the multiple barrier effect at a liquid disposal site with multiple layers of impermeable layers (caprocks) (Miller et al. 1986)

(3) evaluating leakage rates as a function of fault and formation properties.

Figures 8a, b show the distribution, in the form of saturation values, of the  $CO_2$ -rich phase (supercritical  $CO_2$  with small amounts of dissolved water) at the end of the 30-year injection phase and at 500 years, respectively.  $CO_2$  first spreads within the storage formation, both upward and laterally. As indicated by the  $CO_2$  saturation in upper aquifers, the fault zones allow for significant leakage of  $CO_2$  from the storage formation. The upflow of  $CO_2$  in the fault zones is partially diverted sideways into the middle and upper aquifers, which mitigates further upward migration. At the end of the injection phase, the lateral diversion in the middle aquifer is not wide enough to reach the offsetting upper fault zone, and the  $CO_2$  plume is limited to the middle aquifer. After 500 years,  $CO_2$  has

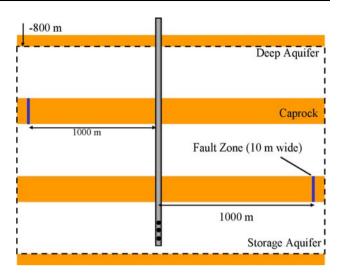


Fig. 7 Model setup for studying effect of multiple caprocks in retarding leakage of CO<sub>2</sub> from storage formation

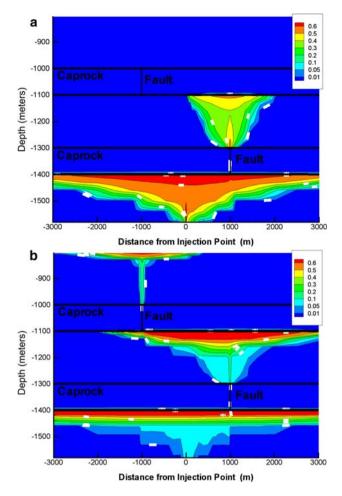
eventually leaked into the upper aquifer, indicating that the lateral extension of CO<sub>2</sub>-phases can lead to leakages through fault zones at a large distance from the spill point. Depending on the geologic and hydrologic conditions, such leakages may occur when the injection period has ended.

#### Caprock effectiveness and hydromechanics

Coupled hydromechanical effects that may have an impact on the effectiveness of caprock include creation of new fractures and changes in apertures of existing fractures in the caprock due to changes in rock stresses or hydraulic pressures. Rugvist and Stephansson (2003) provide an overview of the role of hydromechanical effects for a number of underground industrial activities, including deep injection of liquid waste and CO2. The potential for hydrofracturing caused by injection pressure is a concern for liquid-waste injection, and it is useful to monitor and maintain injection pressure below the lithostatic pressure all through injection operation, to ensure that the pressure is well controlled and hydrofracturing is avoided. For CO<sub>2</sub> injection and storage, it will be comparatively more important to evaluate the associated mechanical effects due to the presence of both the injection and buoyancy pressures.

In the following, we shall discuss hydromechanical processes in the context of CO<sub>2</sub> injection and storage, but similar processes occur for liquid injection without the extra driving buoyancy force. First, injection of CO<sub>2</sub> will result in an increase in formation fluid pressure, especially around the injection source. Such a fluid pressure increase will cause local changes in the effective stress field, which, in turn, will induce mechanical deformations, possibly increasing the porosity and permeability, and thus reducing





**Fig. 8** The distribution of saturation values of the CO<sub>2</sub>-rich phase at the end of the 30-year injection phase (**a**) and at 500 years (**b**)

the fluid pressure. However at the same time, increasing pressure may also cause irreversible mechanical failure in the caprock. This mechanical failure may possibly involve shear-slip along existing fractures and creation of new fractures (hydraulic fracturing), which reduce the sealing properties of the caprock system. Rutqvist and Tsang (2005) and Yamamoto (2006) provided a good overview of the general problem. In addition to these mechanical processes, replacing the native formation fluid with CO<sub>2</sub> may also cause changes in rock mechanical properties through chemo-mechanical interactions between the CO<sub>2</sub> and the host rock, or through desiccation of fractures.

Rutqvist and Tsang (2002, 2005) and Rutqvist et al. (2006a, b) used a code TOUGH-FLAC that they developed to conduct analyses of hydromechanical effects during CO<sub>2</sub> injection in both single-caprock and multilayer systems. For example, in a hypothetical multilayer system, Rutqvist et al. (2006a) studied CO<sub>2</sub> injection for 30 years in a 200-m-thick permeable saline water formation located at 1,600 m depth (Fig. 9). In their model, several layers of

caprocks as well as water-bearing formations were located above the intended storage formation, all of which were intersected by a permeable fault zone. The analysis showed that during injection, CO<sub>2</sub> migrates laterally and upward in the storage formation, driven by injection pressure and buoyancy forces. When the plume encounters the fault zone intersecting the caprock, a considerable amount of CO<sub>2</sub> migrates upward, spreads laterally into the upper overlying zones, and may cause considerable fluid pressure increase there. Based on the changes in effective stresses, the potential for fault slip and fracturing is calculated.

Figures 10 and 11 present, respectively, the results of potential for fault slip and hydraulic fracturing for two different initial stress regimes—a compressional stress regime (horizontal stress larger than vertical) and an extensional stress regime (horizontal stress smaller than vertical). These results are given in terms of pressure margins to the onset of shear slip or fracturing. A positive pressure margin in these figures implies that the local fluid pressure may be above the critical pressure for onset of geomechanical damage. Dark contours indicate areas of the highest potential for onset of shear slip. Results suggest that, once leakage of CO<sub>2</sub> occurs, the potential for fault reactivation and fracturing could be larger in the overlying units than in the storage formation, a result of the smaller in situ stress fields in shallower units. Knowledge of the initial stress regime is very relevant. In the case of a compressional stress regime (Fig. 10), the shear slip is most likely to be initiated in subhorizontal fractures, at the interfaces between the permeable formation layers and the overlying caprocks. In the case of an extensional stress regime (Fig. 11), the shear slip is likely to occur in subvertical fractures in the uppermost aquifer and in the overburden rock. An extensional stress regime may also

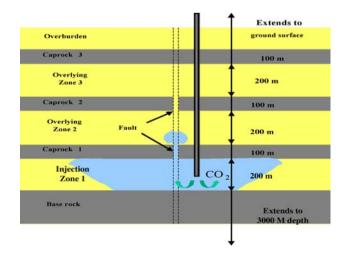


Fig. 9 Model geometry for simulation of hydromechanical effects during  $CO_2$  injection into a multilayered reservoir-caprock system



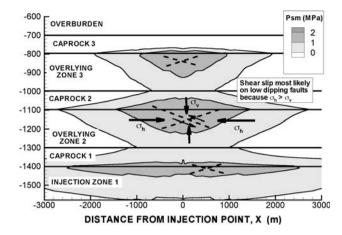


Fig. 10 Calculated pressure margin for shear slip along pre-existing fractures after 30 years of  $CO_2$  injection for compressional stress regime (with magnitude of horizontal stress being 1.5-times the vertical)

allow for hydraulic fracturing at the bottom of the uppermost caprock. The analysis by Rutqvist et al. (2006a) thus demonstrates that for evaluation of the maximum sustainable  $\rm CO_2$ -injection pressure at a particular site, it is essential to have a good estimate of the 3D in situ stress field.

Overall, the various analyses of both single-caprock and multilayered systems show that the magnitude and the anisotropy of the initial stress field is an important factor in determining where and how failure could occur. A site with a horizontal stress much lower than the vertical (i.e., a strongly anisotropic, extensional stress regime) would be most unfavorable for safe and effective CO<sub>2</sub> storage, since subvertical fractures could be more easily reactivated by shear or hydraulic fracturing. A site with a horizontal stress

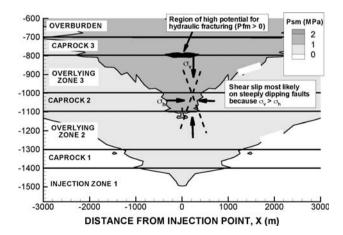


Fig. 11 Calculated pressure margin for shear slip along pre-existing fractures after 30 years of  $CO_2$  injection for extensional stress regime (with horizontal stress magnitude being 0.7 times the vertical). The region of high potential for hydraulic fracturing is also indicated in the figure

approximately equal to the vertical (i.e., an isotropic stress regime) might be the most favorable situation, because an isotropic stress regime tends to prevent shear stress, and hence shear failure along pre-existing fractures, from occurring.

## Site characterization and monitoring

The criteria for selecting a site suitable for  $CO_2$  injection have been discussed by Bachu (2000) and Bachu and Gunter (1999). They are largely similar to those of deep injection of liquid wastes (Warner and Lehr 1977), except for the areal extent at the site being considered for injection and storage. As was mentioned earlier, the scale of  $CO_2$  storage is much larger than that of liquid waste disposal, and also, some leakage into upper layers is allowed, so long as leakage to the atmosphere is limited. This means that characterization of the sites suitable for  $CO_2$  storage has a much larger scope, both horizontally and vertically, than that for liquid waste disposal.

This larger scope can be illustrated using the case studied by Haidl et al. (2005), who conducted a regional geological mapping over a scale of  $200 \times 200$  km, with depth ranging from 1.5 to 3.5 km, for site characterization, as part of a  $CO_2$  storage demonstration project. The objectives of the geological mapping included:

- The distribution of strata comprising the geologic container, identifying and characterizing primary and secondary seals or caprock units.
- Mapping aquifers and aquitards, particularly local thinning or absence of aquitards.
- Determining whether discontinuities are present in the system.

Haidl et al. (2005) used the data generated by their investigation to construct a 3D geologic model that can be used in numerical simulations of risk and performance assessment. This geologic model is also a key ingredient needed to design baseline studies and develop long-term monitoring strategies.

With respect to monitoring of liquid-waste disposal, the need has been discussed by Warner (1992, 1996) and Gerrish and Cooper (1996). The monitoring requirement tends to be very limited. Nearly all the required monitoring (Brasier and Kobelski 1996; Tsang et al. 2002) involves tests and well logs that focus on the mechanical integrity of the injection well and the conditions in the immediate vicinity of the well. The only exceptions are reservoir testing at 1-year intervals to ensure continuing injectivity (i.e., formation permeability having not changed significantly), and recording of operational data such as injection rates and pressures. Furthermore, no monitoring wells away from the injection well are required. There had been



the suggestion that the monitoring wells should be required to perhaps enhance confidence that no migration from the defined disposal zone has occurred. However, Warner (1992) argued that the main hydrologic perturbation caused by liquid-waste injection occurs close to the injection well, and that any monitoring well at some distance away from the well has a high likelihood of missing any of the injection plume, owing to flow-channeling effects caused by formation heterogeneity and the presence of fractures, making such an effort of minor value.

Monitoring of CO<sub>2</sub> injection and storage, on the other hand, is more complex and demanding (see e.g., Lewicki et al. 2005). This is because of the large area covered by the CO<sub>2</sub> plume, and because some level of leakage could be allowed without compromising the atmospheric CO<sub>2</sub> emission reduction goals or endangering the environment. Chalaturnyk and Gunter (2005) have considered the problem in some detail. They advocate that the complete monitoring program should not just involve some measurements over the site area, but rather involve a number of steps:

- Define project conditions.
- Understand the mechanisms that control fluid flow.
- Specify the technical questions to be answered and parameters to be measured.
- Predict the magnitude of changes to be expected in these parameters.
- Select monitoring systems and their implementation locations and frequency.

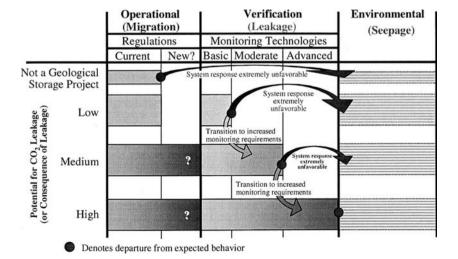
In Fig. 12, Chalaturnyk and Gunter (2005) define three monitoring periods and levels, namely: operational, verification, and environmental. The first and second levels are, respectively, the monitoring needed during the CO<sub>2</sub> injection phase and during the following period of performance confirmation (see also Oldenburg and Unger 2003,

Fig. 12 Monitoring phases, leakage potential, and level of monitoring technologies needed (Chalaturnyk and Gunter 2005) 2004; Oldenburg and Lewicki 2006). The third level, environmental monitoring, includes monitoring of potential seepage to ensure it to be acceptable. The figure also shows the links between the consequences or potentials for leakage and the three levels of monitoring stages. A decision framework has to be developed to provide decision criteria for moving from one level of monitoring to another.

Various monitoring methods, ranging from air-borne surveys, soil gas sampling, in situ tracers, seismic, electromagnetic, ultra-sonic, gravity, to transient-pressure testing methods, are being studied for particular application to  $\rm CO_2$  injection and subsurface migration (e.g., Vrignaud et al. 2006; Strazisar et al. 2006; Mishra et al. 2006; Pickles and Cover 2006; Huang and Fehler 2006). Figure 13 shows the various monitoring methods in perspective (Chalaturnyk and Gunter 2005) according to time frame and the respective needs to monitor migration of  $\rm CO_2$  in the storage formation, leakage of  $\rm CO_2$  upwards, and seepage of  $\rm CO_2$  on the ground surface.

## Effects of CO<sub>2</sub> storage on groundwater resources

Because of the potentially large quantity of CO<sub>2</sub> to be stored, there arises the question of where the displaced in situ brine would flow, with the more specific concern of how that would affect the shallower drinking and ground-water resources. Considerations include, for example, the possible changes in chemical composition of a shallower aquifer resulting from inflow of high-concentration or CO<sub>2</sub>-saturated brine. As discussed in Jaffe and Wang (2003) and Wang and Jaffe (2004), the increased acidity after CO<sub>2</sub> intrusion may enhance the solubility of heavy metals present in minerals or adsorbed on mineral surfaces. Dissolution of heavy metals into the groundwater could then possibly lead to contaminant concentrations above health-based limits. Another concern is the potential impact of





	0.1 – 1 year	1 – 10 years	10 - 100 years	100 – 1000 years
Seepage	Aircraft	Aircraft	Aircraft	Aircraft
	Soil Gas	Soil Gas	Soil Gas	
	Insitu Tracers	Insitu Tracers	Insitu Tracers	Insitu Tracers
Leakage	3D-Seismic	3D-Seismic	3D-Seismic	3D-Seismic
	Tilt Meter	Tilt Meter	Tilt Meter	Tilt Meter
	Pressure	Pressure	Pressure	
	Insitu Tracers	Insitu Tracers	Insitu Tracers	
	Logs	Logs	Logs	
	Passive Seismic	Passive Seismic	Passive Seismic	
Migration	3D-Seismic	3D-Seismic	3D-Seismic	3D-Seismic
	Passive Seismic	Passive Seismic	Passive Seismic	
	X-Well Seismic	X-Well Seismic	X-Well Seismic	
	Tilt Meter	Tilt Meter	Tilt Meter	Tilt Meter
	Pressure	Pressure	Pressure	
		Injected Tracers	Injected Tracers	
	Insitu Tracers	Insitu Tracers	Insitu Tracers	
	Logs	Logs	Logs	
		Injection Rates		

Fig. 13 Monitoring methods according to time frame and the respective needs to monitor (i) migration of  $CO_2$  in the storage formation, (ii) leakage of  $CO_2$  upwards and (iii) seepage of  $CO_2$  to the ground surface (Chalaturnyk and Gunter 2005)

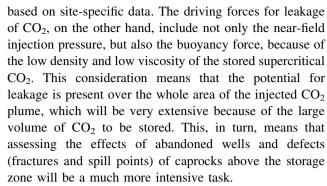
added fluid volumes on surface discharge and recharge of groundwater systems. As an example, Nicot et al. (2006) presented a fictitious case study with CO<sub>2</sub> injection into a deep brine aquifer in the Texas Gulf Coast area, which hydraulically interacts with a distant groundwater regime. On the other hand, these issues are of less concern for liquid waste disposal because they can be readily addressed, due to the relatively small volume and limited area involved.

## Summary and concluding remarks

This paper presents a comparison of hydrologic issues and technical approaches used in injection and disposal of liquid wastes using deep wells, and those associated with injection and storage of CO<sub>2</sub> in deep brine formations.

Overall,  $CO_2$  injection involves more complex hydrologic processes than liquid-waste injection. These complications include effects such as multiphase flow interference and hysteresis in relative permeability functions, as well as much stronger buoyancy flow and flow fingering. However, this may not have practical implications for the performance of a  $CO_2$  injection-storage operation. Additional analyses have to be made to assess the impact at the  $CO_2$  storage scale.

From a practical standpoint, hydrologic concerns for liquid injection are more localized, since the main cause for leakage is injection pressure, which is significantly large only in the area close to the injection well. Within the so-called area of review, strict requirements are necessary for the construction of injection wells and for detection of abandoned wells. As a general rule, numerical modeling is used to estimate the migration of the liquid-waste plume



Hydromechanically, the concern for liquid injection is mainly the potential of hydrofracturing caused by injection pressure around the injection well. For CO<sub>2</sub> injection, the presence of buoyancy pressure implies that the hydromechanical effects on low-permeability caprocks must be assessed along potential leakage paths, all the way from the storage formation to the shallow subsurface. The need can be seen if we consider the significant driving buoyancy force associated with an isolated column of CO<sub>2</sub>, from a storage formation (at, say, 1,000 m) to the land surface. Of course, in practical cases, this column is not isolated and communicates with the shallower brine formations, which would moderate this effect.

An interesting point is that in contrast to liquid waste, a low level of CO<sub>2</sub> leakage into the near-surface environment may not present a serious environmental problem, as evidenced by natural analogs (Lewicki et al. 2006). It has also been mentioned that a useful CO<sub>2</sub> storage system can accommodate such a leakage up to a certain level. Hydrologically, this leads to the question of estimating the potential leakage level of a CO<sub>2</sub> storage system. Such an estimation would require appropriate site-specific data and numerical modeling, It also implies that there is a need for a properly designed site-specific monitoring system, so that any leakage can be detected and evaluated as to whether it is within the range predicted by the model of the site.

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